Use of Combined Electrochemical Approaches for Mineralization and Detection of Hydroquinone Using PbO₂ Electrodes

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Abstract. The electrochemical oxidation (EO) of hydroquinone (H₂Q) has been performed, in acidic media, at PbO₂ electrode by galvanostatic electrolysis applying 10 and 30 mA cm⁻². The concentration of H₂Q during its EO was also monitored by differential pulse voltammetry (DPV) by using PbO₂ electrode. The experimental results of galvanostatic electrolyses showed that the performances of the process remarkably depend on the applied current density and in particular, the removal efficiencies obtained at PbO₂ anode were 100% and 80%, at 30 and 10 mA cm⁻², respectively. Additionally, the electroanalytical technique was efficiently used as a detection method during H₂Q electrooxidation and when DPV analyses were compared with HPLC method, it achieved a good fit, confidence intervals and limits.

Keywords: hydroquinone, electrochemical oxidation, differential pulse voltammetry, electroanalysis.

Introduction

Hydroquinone (1,4-dihydroxybenzene, H₂Q) is an isomer of phenolic compounds (Figure 1), which are considered as environmental pollutants by the US Environmental Protection Agency (EPA) and the European Union (EU) [1]. It is widely used in cosmetics, tanning, pesticides, flavoring agents, medicines, and photography chemicals [2] and can easily be introduced into the environment as pollutants. High concentration of H₂Q can lead to fatigue, headache, and tachycardia to human body and also can damage kidney [3, 4]. Because of its coexistence in environmental samples; efficient, versatile as well as highly sensitive and selective, methods are strongly demanded for the elimination and determination of H₂Q.

In this context, electrochemical technologies have a continuous growing importance in the field of decontamination of effluents [5-8] as well as detection of pollutants. In the former, several anodic materials [6,7], such as boron-doped diamond (BDD) [9-11], lead dioxide [12], tin dioxide [13, 14], platinum, graphite, ruthenium oxide, iridium oxide, etc., have been tested for the destruction of a large variety of model and real wastewaters [6, 7]. However, for the electrochemical approaches for abatement of pollutants, anodes with high oxygen evolution overpotential (i.e. anodes that are poor catalysts for oxygen evolution reaction), such as antimony-doped tin oxide, boron-doped diamond (BDD), or lead dioxide [13-19], favor complete oxidation of the organics to CO₂. Therefore, they are ideal electrodes for wastewater treatment.

For detection analysis, chromatographic and optical methods are preferable over electrochemical methods for detecting and quantifying the pollutants concentration remaining in solution or in the effluent. However, these methods have some drawbacks such as high cost, low sensitivity, insufficient selectivity and long analysis times. Instead, electrochemical methods satisfy many of the requirements for such tasks particularly owing to their inherent specificity, speed of response, more feasible for miniaturization of analysis; sensitivity and simplicity of preparation respect other techniques as chromatographic and spectrophotometric.

Based on this information, we prepared a PbO₂ electrode and this sensor was applied for the quantification of H₂Q during its electrochemical oxidation at Pb/PbO₂ anode in order to demonstrate the applicability of the combined electrochemical technologies for environmental applications as well as its great response respect to chromatographic assays.

Figure 1. Chemical structure of H₂Q.
Experimental

Reagents

Chemicals were of analytical grade, and all solutions were prepared with MilliQ water. Two solutions of H₂O₂ were prepared in 0.5 mol L⁻¹ H₂SO₄, using MilliQ water: (i) 200 mg L⁻¹ (used for electroanalysis procedures as standard solution) and (ii) 50 mg L⁻¹ (used for electrochemical oxidation experiments).

Preparation of PbO₂ electrode

The initial, geometric surface area of the sheet of pure lead, used to prepare the working electrode, was approximately 20 cm². After a deep cleaning of the exposed lead surface [20], the latter was anodized at a current density of 50 mA cm⁻² during an electrolysis time of 1.5 h in a 10% H₂SO₄ solution at 25 °C, in order to oxidize the lead surface into PbO₂ [20-22]:

\[
Pb + SO₄^{2-} \rightarrow PbO₂ + 2e⁻
\]

\[
PbSO₄ + 2H₂O \rightarrow PbO₂ + SO₄^{2-} + 4H^+ + 2e⁻
\]

Surface Analysis

The surface morphology of PbO₂ electrode was investigated by scanning electron microscopy (SEM). These images were performed with SEM PHILLIPS XL-30 - ESEM with Sputter Coater BAL-TEC Model SCD-005.

Analytical methods

Polarization curve measurements were performed using Autolab model PGSTAT320. Pb/PbO₂ was used as working electrode (0.2 cm² of exposed area), Ag/AgCl electrode and Pt wire were used as reference and counter electrodes, respectively, in H₂SO₄ 0.5 mol L⁻¹. During the EO tests, the H₂O₂ concentration of collected samples was determined by differential pulse voltammetry (DPV) with calibration curve. Electrochemical analyses were carried out by using Autolab model PGSTAT320. DPV measurements were usually conducted in the potential window from 0.0 to 1.2 V in H₂SO₄ 0.5 mol L⁻¹. The experiments were carried out at 25°C with a conventional three-electrode system, and applying scan rate of 50 mV s⁻¹; equilibration time of 10 s; modulation time of 0.04 s; initial potential of 0.0 V; end potential of 1.2 V; step potential of 0.006 V; modulation amplitude of 0.05 V and standby potential of 0.05 V. A PbO₂ electrode with an exposed geometric area of ca. 0.8 mm² was used as the working electrode. A platinum wire and an Ag/AgCl (3 mol L⁻¹ KCl) were employed as the auxiliary and reference electrodes, respectively. Calibration curves for H₂O₂ were obtained in 0.5 mol L⁻¹ of H₂SO₄, evaluating the peak intensity as a function of the analyte concentration, and considering at least sixteen analyte concentrations. Every experiment was performed by using a newly prepared electrode, in 30 mL of supporting electrolyte, after that, by adding known volumes of the H₂O₂ solution of 200 mg L⁻¹ in the measuring vessel.

Electrochemical oxidation experiments

Bulk oxidations were performed in undivided electrochemical cell, the reaction compartment having a capacity of 0.4 L, and the solution was stirred by a magnetic stirrer. The experiments of EO of H₂O₂ were performed under galvanostatic conditions by applying 10 and 30 mA cm⁻² using a MINIPA power supply under acidic conditions (0.5 mol L⁻¹ H₂SO₄, for all experiments). PbO₂ was used as anode (a plate with an area of 20 cm²), while a Ti grid was employed as cathode with an inter-electrode distance of 1.5 cm.

Results and discussion

Preliminary electrochemical measurements and surface analysis of PbO₂ electrode

Important information on the electroactivity of anode surface material can be obtained prior to anodic oxygen evolution (o.e.) by polarization curve studies. As it can be observed from Fig. 2, potentiodynamic experiments indicated that Pb/PbO₂ material presents higher oxygen overpotential, which implies that this anode is better electrocatalyst for H₂O₂ oxidation. Analyzing the current densities values used in this work for anodic oxidation of H₂O₂ oxidation, it can be inferred that at 10 mA cm⁻², lower production of hydroxyl radicals could be attained. Conversely, higher values of applied current density favors higher production of hydroxyl radicals, consequently, good performances on electrochemical oxidation must be achieved. This assertion is in agreement with the results reported by other authors [23, 24]. Restricting now our analysis to the behavior of potential (see Fig. 2a), lower values of applied current densities promotes a

![Figure 2](image-url). Polarization curve of PbO₂ electrode in H₂SO₄ 0.5 mol L⁻¹, indicating the values of applied current density used on electrooxidation experiments. Inset: a) behavior of electrical potential of PbO₂ electrode during electrolysis at different applied current densities, b) SEM image of Pb surface before electrodeposition of PbO₂ crystals and c) SEM image of PbO₂ crystals formed.
good potential stability. Conversely, when 60 mA cm$^{-2}$ was applied, the electrical potential was stable in the beginning of the electrolysis, after that, an important increase on potential was observed, indicating instability of the anode surface. However, this behavior will be discussed in next sections.

Regarding the anode surface obtained, Fig. 2b shows the SEM image of lead surface before the electrodeposition of PbO$_2$ with a homogeneous surface without relevant alterations. On the other hand, the amount of PbO$_2$ formed is evident by small PbO$_2$ crystals observed by SEM image, showing the characteristic tetrahedral crystal structure (Fig. 2c).

Electroanalysis methodology: DPV measurements for H$_2$Q

Before EO experiments, standardization and optimization of electroanalytical approach was performed in order to use the PbO$_2$ sensor for the quantification of H$_2$Q during its EO at Pb/PbO$_2$ anode. To estimate electrochemical characteristics of PbO$_2$ electrode and decide the working range of potentials, DPV curves were recorded in 0.5 mol L$^{-1}$ H$_2$SO$_4$ and in solutions containing H$_2$Q.

The working range of potentials was delimited from 0.0 to 1.2 V. Fig. 3 shows the voltammograms of 0.5 mol L$^{-1}$ H$_2$SO$_4$, in the absence (dashed line) and presence of H$_2$Q (bold line), recorded on PbO$_2$ electrode. As can be seen, in the absence of H$_2$Q, no peak was observed. However, in the presence of H$_2$Q, an irreversible oxidation peak at $\approx$0.78 V (vs. Ag/AgCl) was observed on PbO$_2$ electrode, attributed to EO of H$_2$Q. These experiments showed that H$_2$Q is electroactive at this material, its oxidation taking place about 1020-1100 mV before the oxygen evolution reaction (o.e.r.).

A linear relationship between peak current and H$_2$Q concentration was obtained using PbO$_2$ electrode (see Fig. 4). Calibration plot were recorded in a large concentration range to explore the dynamic and linear ranges: after the expected linear tendency at the lower concentration levels the slope diminished up to reach an asymptotic value. Each curve was obtained by evaluating the peak intensity as a function of the analyte concentration, and considering at least sixteen analyte concentrations (inset in Figure 4). The calibration plot was linear between 3.9±0.14 and 50±0.15 mg L$^{-1}$, with regression coefficients always larger than 0.9981. The functional relationship was $i/A=(9.93\pm0.11)\times10^{-7}$ [H$_2$Q] M + (1.56±0.33)×10$^{-6}$ (slope and intercept were the average of six independent calibrations).

Figure 5 also shows that the residuals of the regression are randomly distributed around the zero, allowing a visual verification of the absence of a significant non linearity [25, 26]. It is worth noting that no significant differences in calibration curves recorded in different days were evidenced. A preliminary estimation of the Limits of Detection, LOD, was also possible by using the approach based on the standard deviation of regression [25, 26]: LOD = $3 \times S_{y/x} / b$, where $S_{y/x}$ is the residual standard deviation and $b$ is the slope of the calibration plot. On the basis of the results obtained, a LOD of about 2.05±0.12 mg L$^{-1}$ could be estimated. This approach allows to control both false positive and false negative errors ($a = b = 0.05$) [25].
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Electrochemical oxidation of H₂Q

In order to study the anodic oxidation of H₂Q, a set of galvanostatic electrolysis were performed at 10 and 30 mA cm⁻² at 25 °C. During each electrolysis, samples of anolyte were withdrawn and analyzed by DPV analysis to quantify the concentration of H₂Q remaining in the solution.

As can be seen from Figure 6a, at PbO₂ anode, one of the extreme examples of classical high-oxygen-overpotential material and therefore expected to perform quite well in electrochemical mineralization of organics [6-8, 21, 24], 100% and 80% of mineralization of the initial H₂Q amount in 180 min was attained by applying 30 and 10 mA cm⁻², respectively. From the results reported in Figure 6b, the organic substrate is mineralized, at PbO₂, upon consumption of 4.5 Ah dm⁻³ at 30 mA cm⁻² compared with incomplete elimination attained at 10 mA cm⁻² (~ 2.5 Ah dm⁻³). This experimental evidence supports the idea that the surface of PbO₂ favors the production of *OH radicals, after that, these strong oxidant species react with the organic substrate promoting a fast incineration [12, 24].

Nevertheless, under soft current conditions (10 mA cm⁻²), no enough production of hydroxyl radicals was attained, favoring the formation of hydrated lead dioxide surface, PbO(OH)₂ [12, 21, 23, 24, 27, 28]. This assumption is in agreement with the potentiodynamic measurements showed in Fig. 2.

Based on the existing literature [6, 7, 23, 24], at PbO₂ anode, no H₂Q adsorption is attained, due to “non-active” nature of this electrode, but the organic oxidation clearly involves intermediates that are only available during the oxygen evolution reaction (hydroxyl radicals). Also, the degradation pathway reported by other authors [23, 29, 30] indicated that hydroquinone (H₂Q) is rapidly oxidized to carboxylic acids (scheme). Only one intermediate is previously formed before complete aromatic ring fragmentation, however, this by-product is not enough stable for remain in solution, preferring its oxidation. This assertion is confirmed by no additional peaks observed at DPV analysis, indicating the no eventual formation of hydrobenzoquinone (HBQ) or benzenetriol (BT).

It is important to mention that, for this electrocatalytic material, PbO₂-carboxylic acids interaction can be assumed, the carbonyl groups can exhibit a short-range interaction with surface Pb(IV) sites favoring the elimination of carboxylic acids formed during H₂Q oxidation, as demonstrated by other authors during degradation of diethyl phthalate [21], p-nitrophenol [31], chloranilic acid [32], and glucose [33].

In order to strengthen this statement, the H₂Q concentration decays were analyzed by kinetic equations related to simple reaction orders and good linear correlations were found by using a pseudo-first-order reaction, as presented in inset in the Fig. 7. As can be seen, the apparent rate constants of H₂Q decay (k_app) increases when an increase on applied current density was attained. In fact, the apparent rate constant of 7.3×10⁻³ min⁻¹ at 10 mA cm⁻² passes to 1.1×10⁻² min⁻¹ at 30 mA cm⁻², confirming the higher removal efficiency at higher current density.

As warmly suggested by other authors [25], the analytical procedures were applied by maintaining the analytical system under rigorous statistical control. Thus, the error related with the determination of H₂Q, using DPV and HPLC procedures, was estimated as:

\[
\text{Statistical error (\%) = } \left( \frac{[\text{H}_2\text{Q}]_{\text{HPLC}} - [\text{H}_2\text{Q}]_{\text{DPV}}}{[\text{H}_2\text{Q}]_{\text{HPLC}}} \right) \times 100
\]  

Figure 6. Influence of applied current density, as a function of (a) time and (b) charge passed (Q), on H₂Q decay.

**Scheme 1.** Oxidation pathway of hydroquinone. Hydroquinone (H₂Q), Benzoquinone (BQ), hydrobenzoquinone (HBQ) or benzenetriol (BT).
where $[H_2Q]_{DPV}$ and $[H_2Q]_{HPLC}$ are the concentrations of $H_2Q$ determined with HPLC and DPV, respectively.

As it can be seen in Fig. 8, the DPV gave reliable results, the statistical error being below 5% in the majority, i.e. 98%, of the responses; in addition, it is important to highlight that the average value of $H_2Q$ concentration estimated by DPV, at all currents applied, lies with the concentration of $H_2Q$ expected (obtained by HPLC).

**Conclusions**

In conclusions, it was possible demonstrating the potentiality of the proposed electroanalytical procedure for determining $H_2Q$ during its EO. Such a sensor is characterized by a higher sensitivity and reproducibility and the low limit of detection allows reducing matrix effects by working in highly diluted solutions. Moreover, the proposed procedure is cheaper than the commonly used chromatographic analysis and than other instrumental methods involving more toxic or expensive reagents.

In order to compare the results obtained with the proposed procedures, HPLC experiments were performed to analyze the total amount of $H_2Q$ after electrolysis. Ten samples, during electrolysis at 10 and 30 mA cm$^{-2}$, were collected and analyzed. According to the Student’s t-test, there were no significant differences between the HPLC and electroanalytical procedures at a 95% confidence level.

Restricting now our analysis to EO of $H_2Q$, the present results demonstrate that the process is strongly dependent on the applied current density. Participation of hydroxyl radicals, formed at PbO$_2$ surface, is an important pre-requisite to an efficient mineralization of $H_2Q$, demonstrating that this non-active anode is an ideal material for wastewater treatment.

Finally, the $H_2Q$ solutions after electrolysis, at 10 and 30 mA cm$^{-2}$) were analyzed by electroanalytical methodology reported by Eiband and co-workers [34], and no evidences of pollution by Pb$^{2+}$ were detected. Conversely, when a electrolysis test was performed at 60 mA cm$^{-2}$, the contamination of final solution by Pb$^{2+}$ was achieved. This assumption is confirmed by the electrochemical stability tests performed (see Fig. 2a) before the electrooxidation experiments for elimination of $H_2Q$, where the electrical potential increases when higher values of applied current densities were used. These experiments also confirm the applicability of electrochemical oxidation treatment as an alternative for depollution of effluents using PbO$_2$ anode under soft current conditions to avoid Pb$^{2+}$ pollution.

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Use of Combined Electrochemical Approaches for Mineralization and Detection of Hydroquinone Using PbO₂ Electrodes

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